



**EFFECTS OF RADIATION OF CO<sub>2</sub> LASER ON NATURAL DOLOMITE FOR THE DEGRADATION OF AZO DYE REACTIVE BLACK 5 BY PHOTOCATALYSIS**

**ESTUDIO DE LOS EFECTOS PROVOCADOS POR LA RADIACIÓN DEL LÁSER DE CO<sub>2</sub> EN LA DOLOMITA NATURAL, PARA LA DEGRADACIÓN DEL COLORANTE REACTIVO NEGRO 5 UTILIZANDO LA TÉCNICA DE FOTOCATÁLISIS**

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**Abstract**

In the present work, changes in Natural Dolomite (ND) produced by calcination using a CO<sub>2</sub> (carbon dioxide) laser radiation were analysed, as well as the effect on the degradation and decolourisation of the dye, Reactive Black 5 (RB5), when ND was used as a catalyst. The power density of the CO<sub>2</sub> laser and the duration of irradiation was varied. A mineral analysis was carried out using a scanning electron microscopy (SEM), energy-dispersive spectroscopy (EDS), and X-ray diffraction (XRD). The EDS analysis revealed the presence of elements such as magnesium (Mg), silicon (Si), aluminium (Al), calcium (Ca), oxygen (O), iron (Fe), zinc (Zn) and sodium (Na), while the X-ray diffraction analysis suggested that the treated dolomite samples experienced changes in their crystalline structure when calcined with the CO<sub>2</sub> laser. However, there were no changes in the main phase of the dolomite. Additionally, a photocatalytic study was performed on the degradation and decolourisation of the RB5 in an acid aqueous medium, using ND and ND calcined with the CO<sub>2</sub> laser radiation. Ultraviolet-visible spectrophotometry (UV/VIS) was used for the characterisation of the photocatalytic tests. An increase of 20% in the decolourisation and 19.6% in the degradation of the RB5 was observed.

*Keywords:* dolomite, black 5, photocatalysis, CO<sub>2</sub> laser, laser radiation.

**Resumen**

En el presente trabajo, se analizaron los cambios en la Dolomita Natural (DN) producidos por la calcinación con radiación de láser de CO<sub>2</sub> (dióxido de carbono), asimismo, el efecto en la degradación y decoloración del Colorante Reactivo Negro 5 (CN5) al utilizar DN calcinada como catalizador. Se variaron la densidad de potencia y el tiempo de radiación del láser de CO<sub>2</sub>. Se analizó mediante microscopía electrónica de barrido (MEB), espectroscopia de dispersión de energía (EDS) y difracción de rayos X (DRX). El análisis EDS reveló la presencia de los elementos magnesio (Mg), silicio (Si), aluminio (Al), calcio (Ca), oxígeno (O), hierro (Fe), zinc (Zn) y sodio (Na), mientras que el análisis de DRX sugirió cambios en la estructura cristalina de la DN cuando fue calcinada, sin embargo, la fase principal de la DN se conservó. Además, se realizó un estudio fotocatalítico para la degradación y decoloración del CN5 en un medio acuoso ácido usando DN y DN calcinada con radiación de láser de CO<sub>2</sub>. Se utilizó la espectrofotometría ultravioleta-visible (UV/VIS) para la caracterización de las pruebas. Se observó un aumento del 20% en la decoloración y un 19.6% en la degradación del CN5.

*Palabras clave:* dolomita, negro 5, fotocatalisis, CO<sub>2</sub> láser, radiación láser.

**1 Introduction**

Currently, there are more than 10,000 types of synthetic dyes commercially available, which are used in the textile, cosmetic, food, medicine, and

other industries. The annual production worldwide is approximately 700,000 tons of dyes are produced yearly (Zollinger *et al.*, 1987). Of this amount, approximately 10-15% of the dyes are released into the environment during manufacturing and usage (Vaidya *et al.*, 1982; Sheet *et al.*, 2014).

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Nowadays, the estimated production of colourants worldwide is about 10 million tons yearly, with azo dyes being the most used ones in the textile industry, representing approximately 70% of this production (Behnajady *et al.*, 2007; Mahmoodi *et al.*, 2006). These types of dyes are chemically stable because they contain an azo group, consisting of two nitrogen atoms ( $-N=N-$ ), so they are considered poorly biodegradable. Thus, most of the residual dyes accumulate in lakes and bays and cause a decrease in the amount of sunlight passing through the water, and consequently, induces a decrease in the photosynthetic activity. This in turn decreases the available oxygen content in the ecosystems (Lucas *et al.*, 2006; Kaneva *et al.*, 2016). Traditional wastewater treatments have proved to be remarkably ineffective in the handling of wastewater of the synthetic textile dyeing process, because the treatment of industrial waters can be complicated by the containing of recalcitrant or refractory compounds, whose biological degradation occurs so slowly that it makes inefficient this type of system (Salas. 2010). Other investigations have also addressed this problem using different processes, such as activated carbon absorption (Nematollahzadeh *et al.*, 2015; Al-Degs *et al.*, 2007; Ip. Barford *et al.*, 2010; Vinod *et al.*, 2014; Tawfik *et al.*, 2014), filtration (Ahmad *et al.*, 2007); by means of mesoporous carbon (Mohammadi *et al.*, 2011), using immobilised white rot fungi cells (Martinez. 2017), by core/cell nanoparticles (Vinod *et al.*, 2014), synthesising copper nanoparticles (Manoj *et al.*, 2016), with nanocomposites (Saravanan *et al.*, 2013-2015), using polyamide nanocomposite membrane, containing alumina nanoparticles synthesised in situ with interfacial polymerisation (Tawfik *et al.*, 2012), the removal of hazardous dyes and others compounds using graphene oxide (Robati *et al.*, 2016), by ultrasonic-assisted adsorption (Ghaedi *et al.*, 2015; Arash *et al.*, 2015), oxidisation and degradation (Domenzain *et al.*, 2016), and finally utilising rice husk and its ash as low-cost adsorbents in water and wastewater treatment (Ahmaruzzaman *et al.*, 2011), are some common examples. Even though there are another processes as well, such as an adsorptive removal of dyes through carbon nanotubes; however, it has been observed that these kinds of processes have toxic effects (Vinod *et al.*, 2013). There is also the biosorption process for wastewater treatment but it is focused on the concentration of metal (Vinod *et al.* 2015). Additionally, some researchers have addressed most of the dyes, in particular, the azo dyes, contain carcinogenic properties (Golka *et al.*, 2004).

Studies on advanced oxidation process (AOPs) have demonstrated that it can be a potential technological alternative for the treatment of effluents. AOPs is based on the generation of hydroxyl radicals ( $OH\bullet$ ), which are highly oxidant and non-selective, promoting the degradation of extremely polluting compounds and contributing to their total mineralisation. The  $OH\bullet$  radicals can modify the chemical structure of recalcitrant organic compounds, converting them into simpler compounds with lower molecular mass, contributing to less toxicity for micro-organisms and consequently higher biodegradability (Muruganandham *et al.*, 2004; Giraldo *et al.*, 2004). Within the AOPs, photocatalysis is another technique often used to accelerate the generation of  $OH\bullet$  radicals through photoreaction. It combines hydrogen peroxide compounds ( $H_2O_2$ ) with white light, thereby containing the ability to accelerate the production of  $OH\bullet$  radicals (Vinod *et al.*, 2011; Saravanan *et al.*, 2013). The mechanism occurs through the action of emitted radiation by a white light lamp for the photolysis of  $H_2O_2$  molecules, meaning that the molecule is broken down by photons producing  $OH\bullet$  radicals, as is expressed in Eq. (1).

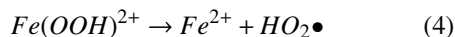
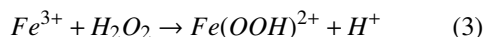
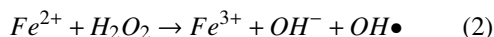


Heterogeneous photocatalysis is a catalytic phenomenon, related to the chemical properties existing at the surface of a solid. It is associated with the adsorption of molecules of a fluid on the surface of a solid, so the oxidation directly takes place on the surface of the particle that is used as a catalyser. Every solid has the property to fix or adsorb the nearby molecules, atoms, or ions on its surface. Adsorption can be produced either by breaking a crystal or using the van der Waals forces. On one hand, the process of breaking a crystal consists the breaking of some covalent bonds, providing one or more free valences to each atom of the surface. The number of nearby atoms existing on the crystal, before the surface formation, generates a decrease, experiencing a set of unbalanced forces; this phenomenon is known as surface free energy. If a molecule with an affinity with these free valences is close enough, an electronic arrangement will occur with the system, similar to that exhibited in a chemical reaction. The result is the fixation of the molecule to the surface, through chemical adsorption or chemisorption. On the other hand, the other recognised form of adsorption is one occurring through the van der Waals forces between atoms, molecules, and the surface. In this case, there is not an electronic arrangement in the system but there are

forces produced by electronic or dipolar attractions. This type of interaction is called physical adsorption or physisorption (Fuentes *et al.*, 1997; Gelover *et al.*, 2014).

The catalytic activities are strongly dependent on the composition, size, and shape of the catalyst. In the photocatalytic technique, irradiation of the semiconductor with a photon of sufficient energy, greater or equal to the band gap energy, could promote an electron from a valence band to a conduction band. As a result, the electron leaves a vacancy behind in the valence band called positive holes, which could oxidise the organic material by the removal of an electron or react with water or hydroxyl forming a powerful oxidant; a hydroxyl radical, as can be seen in Fig. 1. The conduction band electrons reduce dissolved oxygen, producing a superoxide anion radical, which is highly reactive and can oxidise any organic compound (Tawfik *et al.*, 2011; Saravanan *et al.*, 2016).

The Fenton system is one of the most utilised systems, degrading various azo dyes with the hydroxyl radical, generated from the reduction of hydrogen peroxide molecules with Fe (II) ions at acid pH:



The presence of light radiation in the photo Fenton process improves the azo dye degradation efficiency, due to quick photoreduction of the ferric ion to ferrous ion (Vergara *et al.*, 2012; Karthikeyan *et al.*, 2012). The oxidative decolourisation of RB5 has been previously studied, using the processes of Fenton and photo-Fenton, which were found to be effective. Also, the use of mercury lamps at low pressure have been investigated for this purpose.

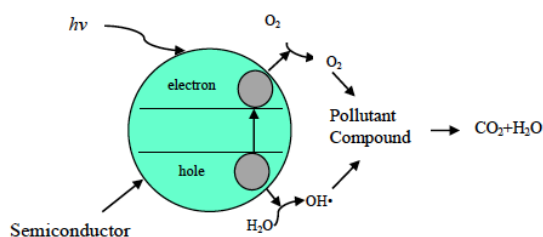


Fig. 1. Scheme of formation of the redox pair in a

particle of the semiconductor.

They exhibited minimal effect in decolourisation, but they were effective for the mineralisation of dyes; the  $H_2O_2$  was also studied. Without the combination with other reagents, it had no influence on the decolourisation of the dye. However, in concentrations of  $2.4 \times 10^{-4}$  to  $9.8 \times 10^{-4}$  mol/L, it increased the decolourisation. Moreover, some researchers have found that the pH of the dye solution has an important impact on the adsorption capacity, significantly the extent of adsorption of the dye is affected, due to the effect of pH on the surface binding sites of the adsorbent, and on the ionisation processes of the dye molecules. An optimum pH of 3 was selected for further investigation. The higher adsorption of the dye, at a low pH is apparently due to greater accessibility of the dye to active sites and more facile diffusion (Mittal *et al.*, 2010; Hadi *et al.*, 2010). Additionally, some investigations for the treatment of contaminated affluent have been carried out using porous materials, either as absorbents or as a catalyst support. For instance, the natural zeolite, which is a porous material calcined at different temperatures, has demonstrated a decolourisation between 80% and 85% and elimination of 50% of RB5 dye. These properties are ascribed to it due to its composition of semiconductors, namely, iron, titanium and zinc (Domenzain *et al.*, 2016). Semiconductors are the commonly used materials in the degradation process of azo dyes. There are several approaches to improve the photocatalytic activity of semiconductors under visible light, such as dye sensibilisation, polymer sensitisation, non-metal doping, metal doping, and coupling of semiconductors. Doping is a generally used method to improve the various properties of semiconductors (Saravanan *et al.*, 2013). Furthermore, Dolomite has been investigated for these purposes. It is a double carbonate of calcium and magnesium,  $CaMg(CO_3)_2$ , containing 30.41% of CaO, 21.86% of MgO, and 47.73% of  $CO_2$  in its purest forms. It is formed by rhombohedral crystals, which are usually deformed. It is very crushed, curved, and compacted in the form of small geodes (dolomites). Usually, it may contain impurities, such as Fe and Mg. Due to its Fe content and porosity, it can be a good catalyst. Fe as an active phase is responsible for the catalytic activity, while the porosity disperses the active phase, stabilising and providing good mechanical properties (Muruganandham *et al.*, 2004; Giraldo *et al.*, 2004; Fuentes *et al.*, 1997).

Some investigations have shown that calcined

dolomite has improvements in its composition and high capacities of absorption when the dolomite is decarbonised through calcination, it produces MgO and increases its specific area, which has been shown to be the main contributor to the elimination of boron (B) (Sasaki *et al.*, 2013). Some of the applications of calcined dolomite are for the treatment of phosphate waters, pentachlorophenol, chromate (Albadarin *et al.*, 2012), Pb<sup>2+</sup>, and reactive dyes (Dobrowolski *et al.*, 1999).

In particular, the CO<sub>2</sub> laser radiation is one of the most used because it is highly efficient, with a high concentration of energy and a potential source of heat due to its monochromatic beam. Also, it has been used to process materials for grain refinement, homogenisation, increasing corrosion and fatigue resistance, and enhancing the micro-hardness in aluminium and titanium alloys (Nagarathnam, 2001; Dutta *et al.*, 2003) as well as being used for improving the mechanical properties in fresh cement paste, by producing fewer pores (Moreno *et al.*, 2011).

The objective of this work was to determine the effects of CO<sub>2</sub> laser radiation on the properties of the ND, and its subsequent use as a catalyst in the degradation and decolourisation of RB5. This material was characterised to determine its global composition, the inner phases, and the presence of iron oxides in the mineral, which is a promoter for the elimination of the RB5 dye using the photocatalysis process. It is also used to identify the power and the duration of irradiation that provides the dolomite better features as a catalyst.

The novelty of this work was to change the conventional way of calcining which is usually done with muffles, the conventional calcination can take hours and generate a considerable expenditure of energy, so it has been proposed to replace the calcination with muffle by calcination with CO<sub>2</sub> laser radiation, which contributes to a considerable saving of energy and time, in addition to the use of dolomite as a catalyst for the degradation of azo dyes.

## 2 Materials and methods

Natural dolomite (ND) in powder was used for the samples. The dolomite used was from Catano-Etla, Oaxaca, México. The zone is corresponding to the Miocene age, approximately from 15 million years (Dobrowolski *et al.*, 1999). The azo dye, Reactive Black 5 (RB5) supplied by Ciba-Geigy® was used for

the photocatalytic process. Hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) stabilized at 30% was used as an oxidizing agent while chlorhydric acid was employed to control the pH of the solution; both compounds were supplied by Fermont®. A commercial light lamp of 25 Watts provided by Tecno Lite® was used to radiate the aqueous solution.

The ND was calcined by using a CO<sub>2</sub> laser radiation of 130 Watts with a wavelength of 10.6 μm. The power densities used were  $I = 1.18 \times 10^6 \text{ W/m}^2$ ,  $I = 1.33 \times 10^6 \text{ W/m}^2$  and  $I = 1.49 \times 10^6 \text{ W/m}^2$  applied at time periods of 5, 10 and 15 s. Thus, nine calcined samples and one more without calcining, denominated as the control sample (CS) were prepared, see Table 1.

The laser set-up used for the calcination process is illustrated in Fig. 2. The important property of the laser treatment is the power density, which determines the kind of laser treatment, represented in the Eq. (5). (Pawlowski, 1999):

$$I = \frac{P}{S} \quad (5)$$

where  $I$  is the laser power density,  $P$  is the laser output power and  $S$  is the beam area.

Table 1. Parameters used for the preparation of the samples.

Sample	Power density $\times 10^6 \text{ [W/m}^2\text{]}$	Calcination time [s]
CS	-	-
S1	1.18	5
S2	1.18	10
S3	1.18	15
S4	1.33	5
S5	1.33	10
S6	1.33	15
S7	1.49	5
S8	1.49	10
S9	1.49	15

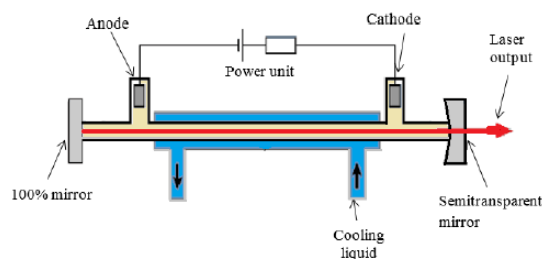


Fig. 2. CO<sub>2</sub> laser set-up used to radiate samples of natural dolomite.

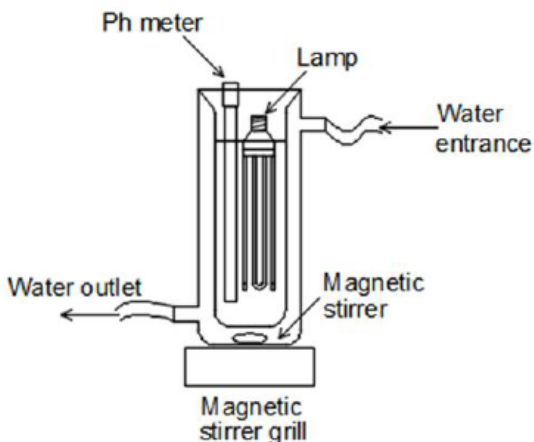


Fig. 3. Schematic view of the photocatalytic reactor assembly.

Furthermore, the ND was evaluated as a catalyser using RB5. For this, H<sub>2</sub>O<sub>2</sub> was used as an oxidising agent and hydrochloric acid to control the pH at 2.5. The aqueous solution was made of 250 ml of distilled water with 50 ppm of RB5 and 20 ppm of each sample, respectively. The solution was constantly agitated using a rotary magnetic bar, keeping a temperature of 20 °C for the whole experiment. The reactor assembly used can be seen in Fig. 3. The reactor was coated with aluminium foil to constrain the light inside the reactor. The spectral data of the catalytic activity were obtained using a UV/VIS variant spectrophotometer, model Cary 1 G, at a scanning speed of 600 nm/min and a wavelength range of 190 to 900 nm. The

degradation of RB5 was monitored for 100 minutes, with 10 minutes intervals for each aliquot. This process was conducted for the ten samples considered.

### 3 Results and discussion

#### 3.1 Energy-Dispersive X-Ray Spectroscopy (EDS)

According to the results obtained by the EDS, the sample was found to be mainly composed of O, Mg, Ca, Si, and Al. Moreover, Si and Al were at the highest percentages meanwhile Na, Fe, copper (Cu) and potassium (K) were at the lowest. The natural sample used had great potential as a catalyser due to its Fe content and porosity.

The results of the EDS analyses for each sample can be seen in Tables 2-4 and Figs. 4-6. The results suggest that the effect of calcination at different power densities and different times did not alter the chemical elements present. However, the percentage weight of each element showed a slight increase. The increase can be attributed to the fact that there was oxidation by the laser heating, producing the combustion of a substance.

The content of Ca and Mg increases for the calcined samples. The Ca/Mg ratio, called relative sensitivity factor, was higher than 1, which suggests that the crude sample was not only composed of dolomite but it also contained other minerals o phases (Sasaki *et al.*, 2013).

Table 2. Percentage weight of the chemical elements obtained by EDS, for a power density of  $I = 1.18 \times 10^6 \text{ W/m}^2$ .

Elements	CS	S1	S2	S3
		Weight [%]		
		5 s	10 s	15 s
O K	50.08	47.01	47.58	49.1
Na K	2.97	0.66	0.75	1.11
Mg K	7.23	6.84	6.31	7.01
Al K	6.03	5.37	5.7	5.32
Si K	14.91	16.5	16.88	16.11
K K	1.3	2.15	2.37	2.11
Ca K	8.01	13.74	13.27	13.76
Fe K	1.42	3.03	3.06	2.7
Cu K	4.4	2.66	2.35	2.77
Zn K	3.64	2.04	1.73	1.96
Ca/Mg	1.11	2.01	2.1	1.96

Table 3. Percentage weight of the chemical elements obtained by EDS, for a power density of  $I = 1.33 \times 10^6 \text{ W/m}^2$ .

Elements	CS	S4	S5	S6
	Weight [%]			
		5 s	10 s	15 s
O K	50.08	48.87	47.38	52.93
Na K	2.97	1.14	0.78	0.56
Mg K	7.23	6.84	6.99	6.89
Al K	6.03	5.41	5.41	5.49
Si K	14.91	15.73	16.49	16.94
K K	1.3	2.1	1.98	2.45
Ca K	8.01	12.85	13.41	15.3
Fe K	1.42	2.45	2.66	2.97
Cu K	4.4	2.71	2.63	2.57
Zn K	3.64	1.9	2.26	2.36
Ca/Mg	1.11	1.88	1.92	2.22

Table 4. Percentage weight of the chemical elements obtained by EDS, for a power density of  $I = 1.49 \times 10^6 \text{ W/m}^2$ .

Elements	CS	S7	S8	S9
	Weight [%]			
		5 s	10 s	15 s
O K	50.08	49.46	48.5	49.66
Na K	2.97	2.56	2.37	2.09
Mg K	7.23	7.3	7.63	7.66
Al K	6.03	5.78	5.94	5.8
Si K	14.91	16.21	16.44	15.91
K K	1.3	1.78	1.93	1.7
Ca K	8.01	11.85	12.06	12.03
Fe K	1.42	2.02	2.32	2.19
Cu K	4.4	2.95	2.97	2.61
Zn K	3.64	2.65	2.21	2.45
Ca/Mg	1.11	1.64	1.58	1.57

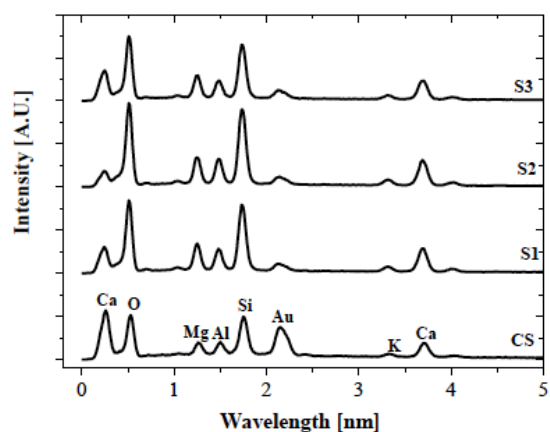


Fig. 4. Distribution of chemical elements obtained by EDS, for a power density of  $I = 1.18 \times 10^6 \text{ W/m}^2$ .

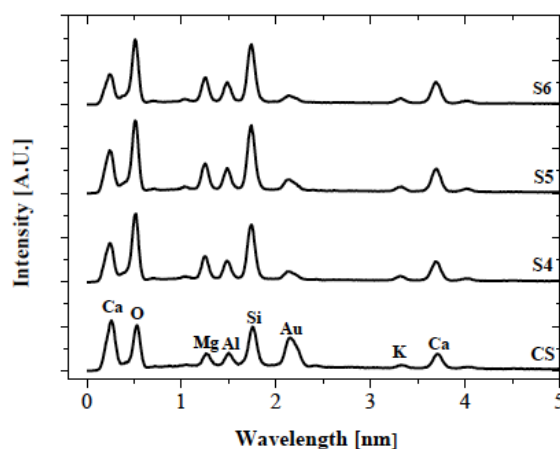


Fig. 5. Distribution of chemical elements obtained by EDS, for a power density of  $I = 1.33 \times 10^6 \text{ W/m}^2$ .

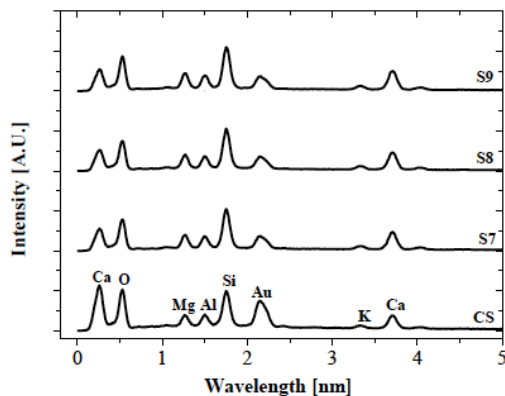


Fig. 6. Distribution of elements obtained by EDS, for a power density of  $I = 1.33 \times 10^6 \text{ W/m}^2$ .

### 3.2 Scanning Electron Microscopy (SEM)

The structural microanalysis of the natural dolomite samples was carried out by SEM. The micrographs of S7, S8, S9, and CS samples are depicted in Fig. 7. It was found that the samples had considerable changes in their structure when they were calcined with the  $\text{CO}_2$  laser radiation.

The best definition of morphology was obtained in the samples prepared at a power density of  $I = 1.49 \times 10^6 \text{ W/m}^2$  for 5, 10 and 15 s, while for the other samples it could not be distinguished. An increase in the porosity and structures, in the form of needles, flat platelets and cubes, and a high formation of particle agglomerates were identified. Also, a more compact structure of platelets and flakes was observed in S8. However, the increase of the structures in the form of needles was remarkable.

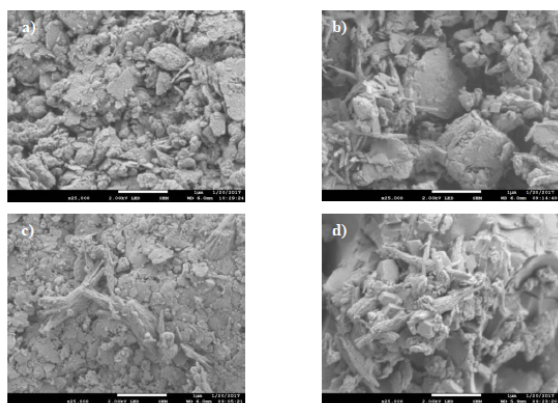


Fig. 7. Micrographs from the samples at  $I = 1.49 \times 10^6 \text{ W/m}^2$ ; a) SC; b) S7; c) S8; and d) S9.

This was possible due to the increase of the temperature, and the effect of the laser radiation, which suggests that each sample exhibited different structures and different sizes due to each particular calcination process.

### 3.3 X-Ray diffraction

The patterns of calcined and uncalcined ND, at power densities of  $I = 1.18 \times 10^6 \text{ W/m}^2$ ,  $I = 1.33 \times 10^6 \text{ W/m}^2$ , and  $I = 1.49 \times 10^6 \text{ W/m}^2$ , at 5, 10 and 15 seconds, are shown in Fig. 8.

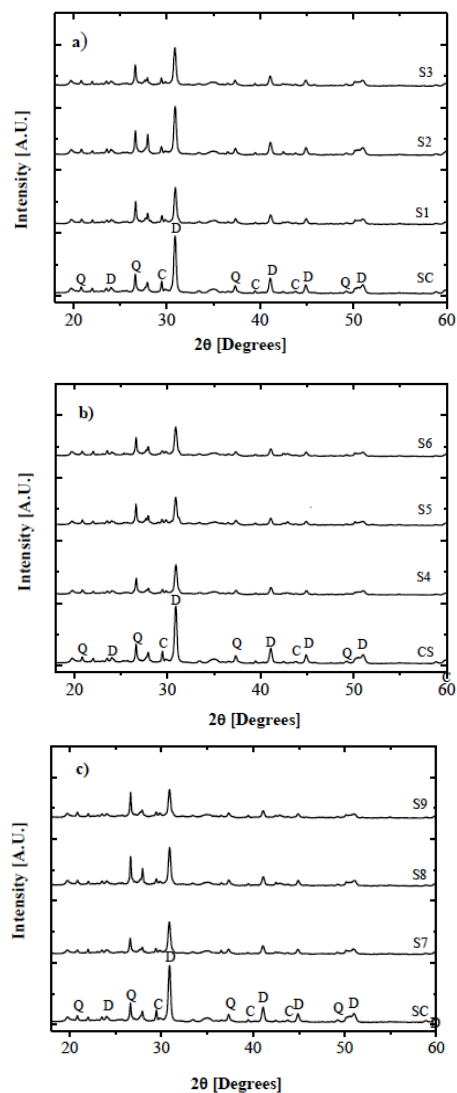


Fig. 8. Diffractograms for the samples prepared at different power intensities; a)  $I = 1.18 \times 10^6 \text{ W/m}^2$ ; b)  $I = 1.33 \times 10^6 \text{ W/m}^2$ ; c)  $I = 1.49 \times 10^6 \text{ W/m}^2$ .

In the analysis, the main phase of dolomite was identified by the characteristic peaks, located in  $2\theta=30.90^\circ$  and in  $2\theta=40.07^\circ$ , the quartz phase, considered as impurities, was located in  $2\theta=26.62^\circ$  and  $2\theta=50.10^\circ$ ; and the phase of calcite, also considered as an impurity, was identified in  $2\theta=29.40^\circ$  and  $2\theta=48.51^\circ$ . In the patterns, low crystallinity with a certain degree of amorphousness was observed. It was determined by the lack of linearity of the baseline of the diffractograms. Besides, it was found that the intensities of the signals changed, due to the increase in the calcination temperature when the samples were radiated, but there were no phase changes in the most intense signals located at  $2\theta=30.90^\circ$  and at  $2\theta=40.07^\circ$ . These signals also decreased, which can be seen in Fig. 8a); b) and c). On the other hand, for the samples prepared at a power density of  $I = 1.33 \times 10^6 \text{ W/m}^2$ . Furthermore, the only phase that showed a decrease in signal (intensity), corresponded to the dolomite. The calcite showed a slight decrease in intensity, while the intensity of quartz was not affected signalling to the characteristic phase.

### 3.4 Calculation of crystal size

The Debye-Scherrer method was used for the crystal size determination, which is generally used to determine the mean diameter of a crystal grain, in the most representative phases involved in the sample studied. For this, one peak was analysed for the dolomite phase and another for the quartz phase. The peak analysed for the dolomite phase, corresponded to the diffraction angle existing in  $2\theta=30.90^\circ$ , meanwhile for the quartz phase it was in  $2\theta=26.62^\circ$ , as seen in Fig. 9.

Table 5. The crystal size of the dolomite and quartz phases.

Sample	Dolomite	Quartz
	crystal size	crystal size
	(nm)	(nm)
SC	26.76	55.26
S1	26.25	59.27
S2	26.42	58.25
S3	26.32	56.48
S4	25.35	51.79
S5	25.58	57.69
S6	25.59	57.13
S7	25.92	51.53
S8	26.71	64.51
S9	26.45	61.68

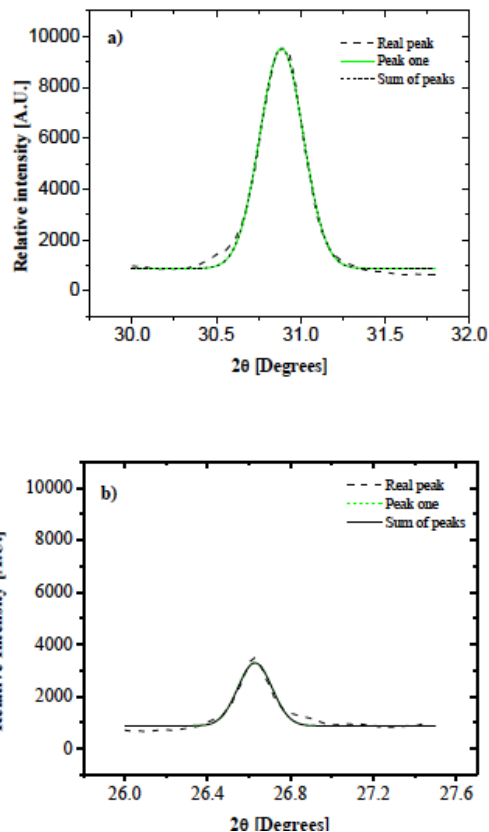


Fig. 9. Diffraction pattern simulation adjusted with a Gaussian distribution; a)  $2\theta=30.9^\circ$  for the dolomite phase; b)  $2\theta=26.62^\circ$  for the quartz phase.

It shows an example of the data obtained for the CS by this method. The results obtained for each sample are reported in Table 5. In both cases, they were adjusted with a Gaussian distribution. To determine the crystal size, Eq. 6 was used.

$$D = \frac{K\lambda}{\beta \times \cos\theta} \quad (6)$$

where  $D$  is the crystal diameter,  $\lambda$  is the X-ray wavelength equal to 0.154 nm,  $K$  is the shape factor with a value of 0.89,  $\beta$  is the full width at half maximum FWHM in radians units and  $\theta$  is the angle measured in degrees.

According to the results obtained for the dolomite crystal diameter, a general behaviour was observed. A slight decrease of particle size for the samples, prepared at  $I = 1.33 \times 10^6 \text{ W/m}^2$  (S4, S5, and S6 samples), with the smallest diameter was found, which means that the crystal size can be reduced by increasing the temperature. On the other hand, for the quartz phase, it showed a slight increase in most cases.



### 3.5 UV/VIS spectroscopy

The UV/VIS spectroscopy technique was used to measure the changes in the absorption bands of RB5 to determine degradation and decolourisation. The process was monitored and evaluated by changing the spectral signals as a function of the reaction time. The hydroxyl radical generated during the photocatalytic process continuously attacked the organic pollutant, through a series of reactions. In this process, the complex organic structure of the pollutant is broken down into smaller intermediates compounds. Moreover, the azo-bond (C–N=N–) is attacked during the photocatalytic dye degradation process, and this destruction of the C–N and N=N bonds leads to colour removal. (Gelover *et al.*, 2014; Stambolova *et al.*, 2012; Aguedach *et al.*, 2005; Damodar *et al.*, 2010; Bauer *et al.*, 2001).

#### 3.5.1 Decolourisation of RB5 dye at the 595 nm band

In Fig. 10, the calibration curve of RB5 is shown. It was generated from different solutions, within the range of 10 ppm to 100 ppm, with intervals of 10 ppm. The amount of light absorbed was measured using a UV/VIS spectrophotometer. The absorption peak at 595 nm, in the visible region, was the band analysed for the chromophores, containing a conjugated  $\pi$  bond using two double azo bonds of the RB5 group, which were used to measure the decolourisation.

The concentration of the colourant in the solution was calculated with the Lambert-Beer law. The values were obtained by segmenting the UV-VIS spectra in a calibration graph at  $\lambda = 595$  nm.

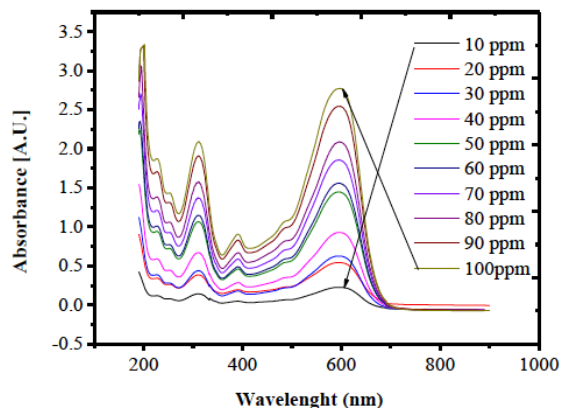


Fig. 10. UV-Visible absorption spectra of RB5 solution during degradation by photocatalysis.

The percentage of decolourisation (%Decolourisation) was calculated by means of Eq. 7 (Dutta *et al.*, 2003; Moreno, 2011; Lucas *et al.*, 2006; Saravanan *et al.*, 2013):

$$\%Decolourisation = \left(1 - \frac{C}{C_0}\right) \times 100 \quad (7)$$

where  $C$  is dye concentration (ppm) at the beginning and  $C_0$  is dye concentration at a determined time. Table 6 summarises all the results in percentage for decolourisation at 595 nm and degradation at 310 nm for each of the calcined samples and the control sample.

Fig. 11a shows the results obtained for the samples prepared at  $I = 1.18 \times 10^6$  W/m<sup>2</sup>. It was observed that the highest percentage of removal was caused in the S2 sample.

Table 6. Percentage of degradation and decolourisation, according to a density of power and duration of irradiation (calcination).

Sample	Power density [W/mm <sup>2</sup> ]	Irradiation time [s]	Decolourisation ( $\lambda = 595$ nm) [%]	Degradation ( $\lambda = 310$ nm) [%]
MC	-	-	67.8	37.8
S1	1.18	5	72.4	36.6
S2	1.18	10	80.7	45.8
S3	1.18	15	72.4	46.7
S4	1.33	5	76.9	46.7
S5	1.33	10	75.6	42.5
S6	1.33	15	86	53.4
S7	1.49	5	72.6	45.2
S8	1.49	10	44	73.9
S9	1.49	15	87.9	57.4

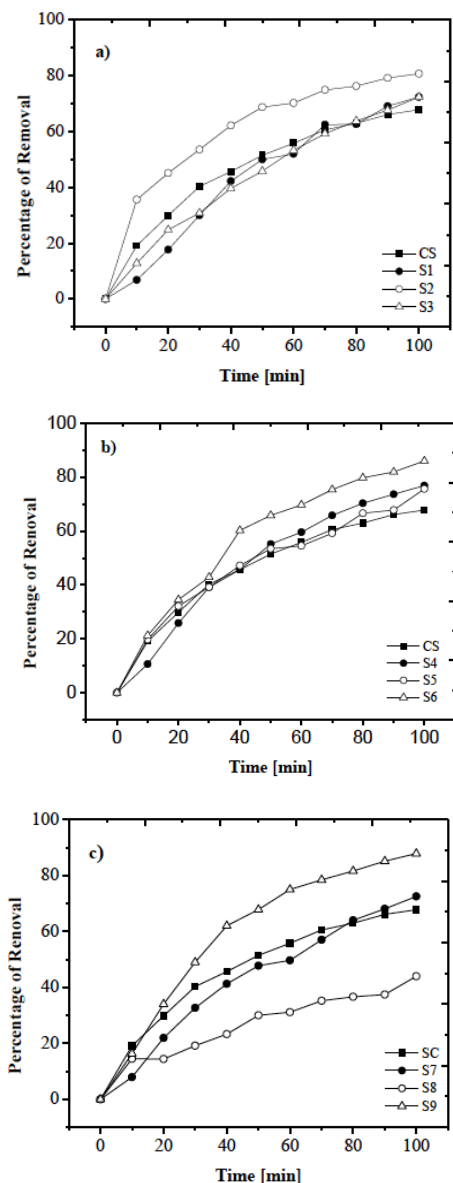


Fig. 11. Comparison of the percentage of removal of samples radiated at different times: 5, 10 and 15 seconds against the control sample for  $\lambda = 595$  nm at different power densities: a)  $I = 1.18 \times 10^6$  W/m<sup>2</sup>; b)  $I = 1.33 \times 10^6$  W/m<sup>2</sup> and c)  $I = 1.49 \times 10^6$  W/m<sup>2</sup>.

The percentage of decolourisation of this sample was approximately 80.70%. On the other hand, the S1 and S3 samples demonstrated a decolourisation percentage of approximately 72.40% for the RB5, similar to the decolourisation exhibited for CS. In the case of the samples radiated at  $I = 1.33 \times 10^6$  W/m<sup>2</sup>, see Fig. 11b, only the sample S6 presented the

highest percentage of removal at 86%; however, the decolourisation kept improving until 50 min of the reaction was completed. The S4 and S5 samples showed 76.9% and 75.6% of decolourisation respectively. Finally, the results for the samples radiated at  $I = 1.49 \times 10^6$  W/m<sup>2</sup> are shown in Fig. 11c. It was observed that the S9 sample exhibited a percentage removal of 87.9%, which was to the highest in comparison with the S7 and S8 samples, presenting percentages of 72.6% and 44%, respectively. The S8 sample was less efficient than CS due to the fact that the sample collapsed in presenting inefficient behaviour as a catalyser.

### 3.5.2 Degradation of RB5 dye at the 310 nm band

The peaks at 310 nm in the UV region were related to the naphthalene rings. In this case, the degradation of the two aromatic structures were also identified, which are assigned to the  $\pi-\pi$  transition of an electron, (Damodar *et al.*, 2010).

The degradation values for each of the samples were obtained by segmenting the UV-VIS spectra in the calibration graph for the degradation peaks at 310 nm. The percentage of degradation (%Degradation) was calculated using Eq. 8, (Tawkik *et al.*, 2012; Luna *et al.*, 2013; Savaranan *et al.*, 2013).

$$\%Degradation = \left(1 - \frac{C}{C_0}\right) \times 100 \quad (8)$$

where  $C$  is dye concentration (ppm) at the beginning, and  $C_0$  is dye concentration at a determined time.

Fig. 12 shows the degradation behaviour of RB5, using the samples studied. In Fig. 12a the behaviour for the samples prepared at the density of  $I = 1.18 \times 10^6$  W/m<sup>2</sup> are shown, the performance was similar for the two samples: S2 and S3, with 45.80% and 46.70% respectively. The least efficient sample was S1, presenting a degradation percentage of 36.60%. It was due to the low radiation time and the low laser power used. In Fig. 12b, the samples were prepared at the density of  $I = 1.33 \times 10^6$  W/m<sup>2</sup>. It can be seen that better behaviour was achieved by S6, with 53.4% of degradation. In Fig. 12c, the degradation achieved in the sample S8, with a power density of  $I = 1.49 \times 10^6$  W/m<sup>2</sup>, can be seen to be 73.90%.

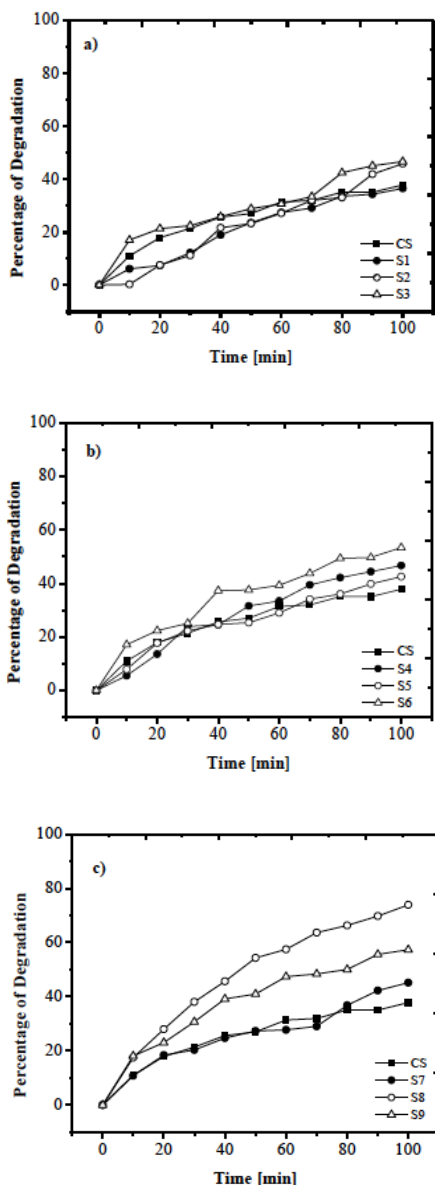


Fig. 12. Comparison of degradation behavior of the samples radiated at the same power density at: a)  $I = 1.18 \times 10^6 \text{ W/m}^2$ , b)  $I = 1.33 \times 10^6 \text{ W/m}^2$  and c)  $I = 1.49 \times 10^6 \text{ W/m}^2$ .

## Conclusions

The use of photocatalysis processes with calcined dolomite, hydrogen peroxide, and white light for decolourisation and degradation of RB5, may represent an opportunity for new applications of the

$\text{CO}_2$  laser radiation, and also for dolomite, since, this material is abundant in nature; it is suitable for its characteristics and its low cost. It was found that the  $\text{CO}_2$  laser radiation is effective for the calcination of ND, since, the results showed that there was greater decolourisation and degradation of the RB5 when ND calcined with  $\text{CO}_2$  laser radiation was used as a catalyst than when ND was used without calcining. The increment was of 20% more in the decolourisation and 19.60% more in the degradation of the RB5 in comparison to the results obtained when the ND without calcining was used. It was seen in the results that the best decolourisation was obtained with the sample that was calcined at a higher power density and with longer irradiation time. On the other hand, the crystal size for the dolomite was maintained in a range of 25.32 nm to 26.76 nm while the range for the crystal size for the quartz was 51.53 nm to 64.51 nm. A more in-depth analysis must be performed that includes aspects of the longest irradiation time and largest irradiation areas, as well as an economic feasibility analysis that determines the potential of this alternative option.

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## Abbreviations

$I$	laser power density, $\text{W/m}^2$
$P$	laser output power, W
$S$	beam area, $\text{m}^2$
$D$	crystal diameter, nm
$K$	shape factor
$C$	is dye time concentration at the beginning, ppm
$C_0$	is dye concentration at a determined, ppm
$\text{H}_2\text{O}_2$	hydrogen peroxide
$\text{OH}\bullet$	hydroxyl radicals
Fe	Iron
AOPs	Advanced Oxidation Process
RB5	Reactive Black 5
ND	Natural Dolomite
s	seconds
ppm	Parts per million

Greek symbols

$\lambda$	wavelength
$\beta$	full width at half maximum: FWHM
$\theta$	angle, degrees
$h\nu$	energy of a photon

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