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# **EFFECT OF AERATION ON THE FERMENTATIVE ACTIVITY OF** Saccharomyces cerevisiae **CULTURED IN APPLE JUICE**

#### EFECTO DE LA AIREACIÓN EN LA ACTIVIDAD FERMENTATIVA DE Saccharomyces cerevisiae CULTIVADO EN JUGO DE MANZANA

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#### Abstract

The influence of aeration on the fermentative activity of *Saccharomyces cerevisiae*RIVE V 15-1-416 was studied in order to evaluate the synthesis of fermentation by-products. To achieve this, the strain was cultured in Erlenmeyer flasks and bioreactor containing sterilized and aroma removed apple juice. The chemical compounds produced during fermentations in shaken (200 min<sup>-1</sup>) and static (without agitation) flasks and bioreactor, all in batch mode, were determined by GC and HPLC. The results showed that agitation of the culture medium dimishes production of total higher alcohols (316.0±27.5mg/L) compared to static cultivation (557.8±28.1mg/L) and enhances slightly ethyl acetate production (75.0±6.5mg/L), whereas on the contrary, the production of acetic acid and glycerol (266.0±8.0mg/L and 2.9±0.2g/L) were higher compared to shaken cultivation (51.0±4.5mg/L and 0.11±0.05g/L) respectively. Batch cultivations carried out in bioreactor with constant air flow of 0.28vvm reported a specific growth rate ( $\mu$ ) of 0.13h<sup>-1</sup> and maximum concentration of ethanol of 42.3g/L during aerobic fermentation. Aeration promotes cell growth, diminishes ethanol yield and, provokes acetic acid uptake and succinic acid synthesis whereas malic acid and ethanol were consumed after sugar depletion. The best results in terms of sensory acceptability of the fermented beverage were obtained when cultivated statically. Aeration control during fermentation with this strain can be used to control the synthesis of chemical compounds of sensory importance.

Keywords: Saccharomyces cerevisiae, alcoholic fermentation, higher alcohols, ethyl acetate, batch cultivation.

#### Resumen

Se ha estudiado la influencia de la aireación en la actividad fermentativa de *Saccharomyces cerevisiae* RIVE V 15-1-416 con la finalidad de evaluar la síntesis de sub productos de la fermentación. Para lograr esto, la cepa se cultivó en frascos Erlenmeyer y en biorreactor conteniendo jugo de manzana estéril y sin aroma. Los compuestos químicos producidos durante la fermentación en cultivo agitado (200 min<sup>-1</sup>), estático (sin agitación) y en cultivo batch fueron determinados por GC y HPLC. Los resultados mostraron que la agitación del medio de cultivo disminuye la producción total de alcoholes superiores (316.0±27.5mg/L) comparado al cultivo estático (557.8±28.1mg/L) y mejora ligeramente la producción de etil acetato (75.0±6.5mg/L), mientras que por el contrario, la producción de ácido acético y glicerol (266.0±8.0mg/L y 2.9±0.2g/L) fueron mayores comparado al cultivo agitado (51.0±4.5mg/L y 0.11±0.05g/L) respectivamente. Cultivos batch realizados en biorreactor con flujo constante de aire de 0.28vvm reportaron una tasa específica de crecimiento ( $\mu$ ) de 0.13h<sup>-1</sup> y una máxima concentración de etanol de 42.3g/L durante la fermentación aerobia. La aireación promueve el crecimiento celular, disminuye el rendimiento de etanol y provoca la toma de ácido acético y la síntesis de ácido succínico, mientras que el ácido málico y etanol fueron consumidos después del agotamiento de los azúcares. Los mejores resultados en términos de aceptabilidad sensorial de la bebida fermentada fueron obtenidos cuando se cultivo estáticamente. El control de la aireación durante la fermentación puede ser usado para controlar la síntesis de ácido succínica.

Palabras clave: Saccharomyces cerevisiae, fermentación alcohólica, alcoholes superiores, etil acetato, cultivo por lote.

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## 1 Introduction

The capability of Saccharomyces cerevisiae to ferment rapidly sugars is used in different technological applications, such as beer, bread, wine and, industrial ethanol productions. S. cerevisiae is facultatively fermenting yeast. Depending on the oxygen and glucose concentration in the medium this yeast shows different metabolic behaviour. Thus, under anaerobic or oxygen-limited conditions it exhibits alcoholic fermentation (Van Dijken and Scheffers, 1986). Moreover, S. cerevisiae is one of the few yeasts with capacity to grow rapidly under anaerobic conditions (Visser et al., 1990). Under fully aerobic conditions a mixed respiro-fermentative metabolism is observed (Crabtree-positive effect) when the sugar concentration exceeds a certain threshold value (approx. 1 mM) (Verduyn et al., 1984; Kappeli, 1986; Verduyn, 1991). Conditions leading to sugar fermentation results in the formation of ethanol, acetic acid, glycerol and other compounds and consequently it reduces the biomass yield (Beudeker et al., 1990). A fully respiratory sugar metabolism can only be achieved aerobically in fed batch cultivation or cultures grown under sugar limitation in chemostat at specific growth rates lower than two-thirds of the maximum specific growth rate on glucose, i.e. 0.44 h<sup>-1</sup>(Petrik et al., 1983; Sonnleitner and Kappeli, 1986; Postma et al., 1989; van Dijken et al., 1993; Paalme et al., 1997). Molecular oxygen serves mainly as final electron acceptor during respiration of glucose but also it is necessary in several biosynthetic pathways, such as those for heme (prosthetic group), sterols, unsatured fatty acids, pyrimidines and deoxyribonucleotides synthesis (Andreasen and Stier, 1953; Nagy et al., 1992; Rosenfeld and Beauvoit, 2003; Snoek and Steensma, 2006). The respiratory metabolism of S. cerevisiae yields approximately 16 ATP per mol of glucose consumed (Verduyn et al., 1991; Pronk et al., 1994). This results in a yield of 0.50 g biomass per g glucose (Verduyn et al., 1991; Pronk et al., 1994). Under fermentative conditions the yield is only two ATP per mol of glucose and consequently, the biomass yield of purely fermentatively growing cells is only 0.10 g biomass per g glucose (Verduyn et al., 1990).

When *S. cerevisiae* is grown under anaerobic conditions, all metabolites of the glycolysis except 2-phosphoglycerate, 3-phosphoglycerate and phosphoenolpyruvate and those of the tricarboxylic acid cycle are in high concentrations as compared with aerobic conditions. Presence of only 0.5-1% vol. O<sub>2</sub> in the inlet gas reduces the concentrations of

these metabolites (Wiebe et al., 2008). In addition, regarding to the activity of the pentose phosphate pathway, if the amount of oxygen available for cellular metabolism is reduced, the relative flux through this pathway diminishes and the flux through glycolysis increases (Gombert et al., 2001; Fiaux et al., 2003; Franzen, 2003; van Winden et al., 2005). Additionally, when S. cerevisiae is grown on glucose in batch culture under aerobic conditions, a certain part of the glucose is initially fermented to ethanol, which, in a separate second growth phase, serves as a carbon and energy source (Fiechter et al., 1981). Ethanol uptake rate and respiration decrease as the concentration of oxygen in the medium diminishes (Wiebe et al., 2008). During glucose metabolism reduced coenzymes (NADH) are produced and in order to maintain the redox balance inside the yeast cell, it must be reoxidized (NAD<sup>+</sup>).

Anaerobically, the only means by which S. cerevisiae can reoxidize surplus production of NADH is by glycerol production (Nordstrom, 1968; van Dijken and Scheffers, 1986; Albers et al., 1998). Under aerobic conditions, several systems for transporting excess of cytosolic NADH to the mitochondrial electron transport chain exist in S. cerevisiae (Luttik et al., 1998; Small and McAlister-Henn, 1998; Larsson et al., 1998). Moreover, glycerol may be also utilized as a carbon source under aerobic conditions by many veasts. Acetic acid is normally produced during alcoholic fermentation; its accumulation would be a consequence of the insufficient activity of acetyl-CoA synthase required to completely oxidize acetate produced from acetaldehyde (van Urk et al., 1990).

## 2 Production of sensory important compounds by Saccharomyces cerevisiae

During alcoholic fermentation many chemical compounds of sensory importance are synthesized by *S. cerevisiae*. These compounds include esters, higher alcohols, organic acids, aldehydes, etc. Esters are the most important flavour compounds in many alcoholic beverages including beer and wine (Suomalainen, 1981). In order to produce esters, ethanol or higher alcohols, fatty acids, co-enzyme A (CoASH) and ester synthesizing enzyme are necessary (Nordstrom, 1962). Esters are formed intracellularly (Nykanen *et al.*, 1977) and, depending on their chain length, they diffuse outside the yeast cell (Nykanen *et al.*,

1977; Suomalainen, 1981). Several types of alcohol acetyltransferase (AATase) are responsible for ester synthesis (Yoshioka and Hashimoto, 1983; Fujii et al., 1996). During the synthesis of acetate esters, the acetyltransferases react with acetyl coenzyme A (acetyl-CoA) and, depending on the degree of affinity, with ethanol or higher alcohols (Nordstrom, 1962; Peddie, 1990; Yoshioka and Hashimoto, 1981; 1983). The synthesis of acetate esters such as isoamyl acetate and ethyl acetate by Saccharomyces cerevisiae during fermentation is ascribed to at least three acetyltransferase activities, namely alcohol acetyltransferase (AAT), ethanol acetyltransferase and iso-amyl AAT (Malcorps and Dufour, 1987; Minetoki et al., 1993; Lilly et al., 2000). It is believed that these enzymes may be involved in very different functions, including cellular fatty acid homeostasis and detoxication mechanisms. It was also reported that AATase activity is strongly inhibited by trace amounts of oxygen or by addition of unsaturated fatty acids to the medium (Yoshioka and Hashimoto, 1981, 1983).

Higher alcohols are quantitatively the largest group of aroma compounds in many alcoholic beverages (Amerine et al., 1980). They are identified by a strong, pungent smell and taste and can have a significant effect on the sensorial quality and character of wines (Rapp and Mandery, 1986; Pretorius and Hoj, 2005; Swiegers and Pretorius, 2005; Swiegers et al., 2005). Higher alcohols are produced either catabolically from the degradation of imported amino acids or anabolically via the biosynthetic route from the carbon source (Hammond, 1993). The amino acids are converted to their corresponding  $\alpha$ -keto acids by transamination (leucine to  $\alpha$ -oxoisocaproic acid, valine to  $\alpha$ -oxoisovaleric acid, and isoleucine to  $\alpha$ -oxo- $\beta$ -methylvaleric acid) (Dickinson and Norte, 1993; Dickinson et al., 1997). Alternatively, these  $\alpha$ -oxo acids can be generated through the breakdown of glucose (Dickinson et al., 1997). Higher alcohols are then synthesized from the corresponding  $\alpha$ -oxo acids by decarboxylation and reduction (Dickinson et al., 1997, 2000). The supplement of oxygen and the increase of temperature during fermentation enhance the production of higher alcohols since it increases the metabolism and as consequence it promotes the cellular growth (Barker et al., 1992).

The present manuscript reports on the effect of aeration on the fermentative metabolism and production of compounds of sensory importance by *Saccharomyces cerevisiae* RIVE V 15-1-416 cultivated in apple juice. In our experiments we considered basically three conditions of cultivation taking into account their technological importance; first when fermentation is carried out under very poor oxygen conditions (oxygen limited static cultivation), then under oxygen limited condition (agitated cultivation in shaker), depending on the speed of agitation and third when air is supplied to the medium (in bioreactor) with a constant flow rate (aerobic culture).

## 3 Material and methods

#### 3.1 Microorganism and maintenance

Yeast strain *Saccharomyces cerevisiae* RIVE V 15-1-416 acquired from the collection of yeasts of the former Research Institute of Viticulture and Enology of Bratislava, Slovak Republic was used in the experiments. The strain was maintained on malt extract agar at 7 oC and reinoculated each three months.

# 3.2 Synthesis of compounds of sensory importance

In the experiments there was used concentrated, sterile and aroma free apple juice acquired from Severofrukt a.s., Terezin, Czech Republic. It was reconstituted with sterilized water until obtaining a total sugar concentration of 12.8%(w/v) and a corresponding pH 3.8 (Downing, 1988). Fermentations were carried out in agitated and in static (without agitation) modes at 28oC in 500 ml Erlenmeyer flasks containing 250 ml of medium. Fermentations carried out in shaken flasks on an orbital shaking machine (200min<sup>-1</sup>) during 8 days and those cultivated statically were left running for 15 days. All experiments were realized at 28oC. Inoculum propagation was carried out in 100 ml of sterile apple juice at 28 oC during 24 hours. The flasks were shaken at 200 min<sup>-1</sup> in an orbital shaker. Cells were separated by centrifugation (3000 min<sup>-1</sup> during 10 minutes) and then washed three times with sterile physiological solution. Fermentation media were inoculated with cells (approx. 1.0±0.1 grams based on wet weight) obtained immediatelly after centrifugation.

#### 3.3 Batch cultivation in bioreactor

Apple juice of Rubin variety containing 13% (w/v) of total sugars and pH 3.8 was utilized in the experiments.

The apples were acquired from CZ-fruit, Prague-CR. The juice was extracted by pressing and then placed in 10 L glass containers. Pasteurization of the juice was done in order to eliminate the microflora and volatile compunds (El-Nemra *et al.*, 1988; Su and Wiley, 1998). Subsequently, the juice was supplied with 1.2 g/L KH<sub>2</sub>PO<sub>4</sub> and 1.2 g/L (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> as phosphorus and ammonium sources in order to promote the growth of the yeast cells.

Cultivations were carried out in 1.5 L apple juice contained in a 2 L bioreactor (BIOSTAT-B.Braun International, Germany). The bioreactor was equipped with a pH-meter, thermometer and dissolved oxygen monitor. The bioreactor was connected to a control micro-DCU-300. The parameters which were kept constant during the whole process were: temperature 18oC, stirring frequency 300 min<sup>-1</sup> and, air flow rate 0.28vvm (for oxygen 0.053vvm). Cultivation time was determined by the increase of the dissolved oxygen value to its initial saturation value then the cultivation was stopped.

The inoculum was propagated in 80 ml synthetic medium of the following composition: glucose 8.0 g/L; peptone 10.0 g/L; KH<sub>2</sub>PO<sub>4</sub> 1.2 g/L; (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> 1.2 g/L and yeast extract 10.0 g/L. The pH was adjusted to 3.8. Cell propagation was carried out in an orbital shaker at 150 min<sup>-1</sup> during 48 hours at 28oC. Subsequently, the cells were separated by centrifugation (3000 min<sup>-1</sup> during 10 minutes), washed with sterile physiological solution and finally inoculated into the bioreactor.

### 3.4 Analytical methods

Volatile compounds (higher alcohols and esters) produced during fermentation were analyzed by GC (Hewlett-Packard 5890II), equipped with a HP5 column (30m x 0.32mm) and FID detector. The samples were centrifuged and then filtered through 0.45  $\mu$ m micro-membranes. Analyses of volatile compounds were performed using the method of dichloromethane micro extraction (Ortega *et al.*, 2001). Finally 1  $\mu$ l of each extract was injected into the column of the equipment.

Acetic, succinic and malic acid, ethanol, glycerol, fructose and glucose were analyzed by HPLC (Pump LCP 4000), equipped with a repacking Watrex 250 x 8mm column (Ostion LGKS 0800 H<sup>+</sup> form) and a RID detector. The conditions of analysis were: column temperature 80°C, mobile phase 5mM H<sub>2</sub>SO<sub>4</sub>, flow rate 1ml/min. The samples after centrifugation (at the rotational frequency of 10000min<sup>-1</sup>) and filtration were diluted with demineralized water (1:3) before injecting to the equipment.

Cellular biomass was determined by gravimetry. Cells were separated by centrifugation (3000 min<sup>-1</sup> during 10 minutes), then washed three times with distilled water, dried at 110°C during 2 hours and finally weighed. Additionally, the yield of biomass and ethanol ( $Y_{X/S}$  and  $Y_{E/S}$ ) and, the specific growth rate ( $\mu$ ) were determined (van Hoek *et al.*, 1998).

### 3.5 Sensory and statistical analyses

Sensory assessment of samples of fermented apple juice was performed using descriptive and preference tests. Attributes such as taste, aroma and odor were evaluated using a Hedonic scale of 5 points (1=dislike extremely and, 5=like extremely). Samples were evaluated by a trained panel of 10 judges. The sensory evaluation was done according to Meilgaard *et al.* (1999). The sensory evaluation data were presented as means of the judge's score. A standard *t-test* was used to test for the statistical significance (P < 0.01) of the differences observed between the scores of the two fermented beverages (cultivated in agitation and statically). Statistical analysis was done using Statistica v.8.0 software.

### 4 Results and discussion

# 4.1 Cultivation under static and agitated conditions

When cultivating yeast Saccharomyces cerevisiae in fruit juices, in media with high sugar content the fermentation always occurred even when oxygen is present in sufficient concentration in the medium. Oxygen is necessary to improve the metabolism of Crabtree positive yeast and so to successfully complete the fermentation. Results showing formation of chemical compounds during fermentation by S. cerevisiae RIVE V 15-1-416 in static and agitated cultivations are shown in Table 1. Additionally, there are also shown compounds analyzed in ciders produced with different strains of Saccharomyces cerevisiae. Marked difference was observed in production of glycerol in static (2.9±0.2g/L) and agitated  $(0.11\pm0.05g/L)$  cultivations. Aerobic conditions would promote cellular respiration and so diminishing the glycerol production. It was reported that, its production would be a response to the osmotic stress as yeasts are cultured in presence of high sugar concentration. From the technological point of view a higher production of glycerol is required since it influences positively the sensory quality of alcoholic beverages; so it imparts a slightly sweet taste (Nieuwoudt *et al.*, 2002).

Higher alcohols are important because of their detrimental impact on the sensory quality of fermented beverages, however a few exceptions exist. But at low concentrations they would contribute positively to the flavor and taste of cider, wine and beer for instance. In this study, it has been observed lower production of total higher alcohols in agitated cultivation (316.0±27.5mg/L) in comparison with static one (557.8±28.1mg/L). In this case, very low amount of oxygen (static cultivation) seemed to enhance the production of higher alcohols. Several authors reported that oxygen promotes the respiratory metabolism and as consequence a higher flux of glucose and amino acids whose break down produces intermediary compounds ( $\alpha$ -cetoacids) for the higher alcohol synthesis (Ribereau-Gayon et al., 1975; Valero et al., 2002). In results of these experiments, production of higher alcohols would also depend on the yeast strain itself. From the sensory point of view, concentrations of higher alcohols higher than 400mg/L would contribute negatively to the organoleptic quality of wines (Rapp and Mandery, With exception of 2-phenylethanol which 1986). imparts a floral aroma (Ribereau-Gayon et al., 2006), whose perception threshold is 10mg/L (Rous et al., 1983), the rest of higher alcohols imparts unpleasant sensory characteristics (Rapp and Mandery, 1986; Ribereau-Gayon et al., 2006). The physiological function of higher-alcohol production by yeast is unclear. It has been suggested that, physiologically, oxidative deamination of amino acids provides the yeast with a mechanism for obtaining nitrogen when its pool has become depleted (Vollbrecht and Radler, 1973). It was also suggested that higher-alcohol synthesis contributes to the maintenance of the redox balance in the cell because the final reduction step in higher-alcohol production involves the reoxidation of NADH+H+ to NAD+ (van Dijken and Scheffers, 1986; Quain, 1988; Zoecklein et al., 1995). However, it has also been stated that there appears to be enough acetaldehyde to maintain the redox balance and that the formation of higher alcohols is not considered to be an important means for the reoxidation of NADH (Boulton et al., 1995). Finally, it has been also suggested that higher alcohol production might act as a detoxification process for the intracellular medium of  $\alpha$ -keto acids and aldehydes, or as a means of regulating the metabolism of amino acids (Ribereau-Gayon *et al.*, 2000). Riberau-Gayon *et al.* (1975) reported that 10% of total higher alcohols is synthesised from corresponding amino acids, 65% from other amino acids and 25% from sugars. *Saccharomyces cerevisiae* yeasts produce active amyl alcohol, isoamyl alcohol and isobutyl alcohol from isoleucine, leucine and valine respectively (Dickinson *et al.*, 1997, 1998, 2000). On the other hand, it was reported that a major conversion of sugars during fermentation provides a higher concentration of higher alcohols in cider (Mangas *et al.*, 1994).

Esters are undoubtedly the most important aroma compounds in alcoholic beverages; their presence determines the sensory quality. Ethyl acetate is probably the most important due to its high concentration compared to the rest of acetate esters. It imparts a light-fruity or solvent-like aroma depending on its concentration. Ethyl acetate is mainly produced using acetyl-CoA as a substrate instead of acetate in Saccharomyces cerevisiae cells (Yoshioka and Hashimoto, 1981). Results of this study showed that agitation enhanced slightly production of ethyl acetate (75.0±6.5mg/L) compared to static fashion  $(51.0\pm6.0 \text{mg/L})$ . Ethyl acetate formation is related to the availability of acetyl-CoA, ethanol and alcohol acetyltransferases necessary for its synthesis (Yoshioka and Hashimoto, 1981; Rojas et al., 2002). Swiegers and Pretorius (2005) reported that the rate of ester formation depends on the concentration of precursors and on the activity of the enzymes involved in the synthesis and hydrolysis. Nevertheless, others factors should also be involved in the synthesis such as for example the type of strain and the initial oxygen concentration in the medium. Additionally, acetate esters are produced in high concentrations during the early stage of fermentation (Henschke and Jiranek, 1993). From the sensory point of view, ethyl acetate concentrations lower than 80 mg/L would contribute positively to the flavour and taste of wines (Ribereau-Gayon, 1978). On the contrary, concentrations over 200 mg/L would impart a vinager taste (Dequin et al., 2003). In addition, fatty acid ethyl esters such as ethyl decanoate (floral odor) are also important for the overall bouquet. The role of ester production in yeast metabolism is also unclear. It is believed that esters might be formed to remove toxic fatty acids from the yeast cell (Nordstrom, 1962, 1964), whereas it has been also proposed that esters could simply be overspill products from the sugar metabolism of yeast during fermentation and might be of no advantage to the yeast cell (Peddie, 1990).

		elders and app	ie juices are shown.		
Compounds (mg/L)	Type of cultivation of <i>Saccharomyces cerevisiae</i> <sup>a</sup>		Compounds analyzed in cidres fermented with	Compounds analyzed in apple juices	
	Agitated	Static	Saccharomyces cerevisiae		
	Mean $\pm$ SD	Mean $\pm$ SD	Mean $\pm$ SD	Mean $\pm$ SD	
Glycerol *	$0.11 \pm 0.05$	$2.9 \pm 0.2$	$4.05 \pm 0.13^1$ ; $2.59 \pm 1.7^2$	$0.0^{5}$	
1-Propanol	$6.0 \pm 1.5$	$27.0\pm4.0$	$20.01 \pm 0.351$ ; $27.3 \pm 13.0^2$	$7.0^{6}$	
1-Butanol	$17.4 \pm 2.5$	$8.6 \pm 1.5$	$6.99 \pm 0.04^1$ ; $6.1 \pm 0.7^2$	$4.50 \pm 0.23^4$	
2-Butanol	$2.0 \pm 0.5$	$1.5 \pm 0.4$		_	
2-Methyl-propanol	$47.0\pm5.0$	$70.0 \pm 5.0$	$22.17 \pm 0.08^{1}; 34.8 \pm 8.9^{2}$	$0.75 \pm 0.04^4$	
3-Methyl-butanol	$123.0\pm8.0$	$268.0\pm8.0$	$232.00 \pm 13.80^3$	$2.11 \pm 0.11^4$	
2-Methyl-butanol	$93.0 \pm 5.0$	$159.0\pm5.0$	$94.8 \pm 0.2^+; 173.0 \pm 41.1^+$	$9.0^{6}$	
2-Phenylethanol	$27.0\pm5.0$	$22.0\pm4.0$	$7.8 \pm 0.39^1$ ; 131.5 $\pm 55.3^2$	$0.46 \pm 0.02^4$	
Ethyl acetate	$75.0 \pm 6.5$	$51.0 \pm 6.0$	$231.06 \pm 33.09^{1}$ ; 114.6 $\pm 35.5^{2}$	$0.57 \pm 0.03^4$	
Butyl acetate	n.d	$5.0 \pm 1.2$	$0.27 \pm 0.02^4$	$0.58 \pm 0.03^4$	
Isoamylacetate	n.d	n.d	$16.66 \pm 1.0^4$	$2.48 \pm 0.12^4$	
Ethyl decanoate	$5.9 \pm 2.0$	$5.3 \pm 0.8$	$1.50 \pm 0.09^4$	$0.01 \pm 0.002^4$	
Acetic acid	$51.0 \pm 4.5$	$266.0\pm8.0$	$900.0 \pm 140.0^1$ ; $282.93 \pm 16.9^4$	$0.0^{5}$	
Succinic acid*	$1.32\pm0.10$	$0.77\pm0.15$	$200.0 \pm 30.0^1; 0.5 \pm 0.06^2$	$0.0^{5}$	

Table 1. Compounds of sensory importance produced by *Saccharomyces cerevisiae* RIVE V 15-1-416 cultivated in apple juice at 28°C in static and agitated cultivation. Furthermore, typical compounds found in ciders and apple juices are shown.

\*g/L., tr.: traces., n.d: not detected., <sup>*a*</sup>Results obtained in this study. <sup>1</sup>Values found in ciders fermented by *S. cerevisiae* (Suarez *et al.*, 2005). <sup>2</sup>Values found in ciders (Picinelli *et al.*, 2000). <sup>3</sup>Values found in ciders fermented by S.cerevisiae (Jarvis *et al.*, 1995). <sup>4</sup>Average values (Wang *et al.*, 2004). <sup>5</sup>Average values (Cabranes *et al.*, 1998). <sup>6</sup>Average values (Souci *et al.*, 2000). <sup>+</sup>Amylic alcohols: 3-Methyl-butanol+2-Methyl-butanol (Suarez *et al.*, 2005; Picinelli *et al.*, 2000). Not reported compounds (-).

Acetic acid is a very important compound; it contributes to the total volatile acidity in wines and ciders. In this study, its production was higher in static cultivation (266.0±8.0mg/L) compared to agitated one (51.0±4.5mg/L). Cultivation conditions leading to alcoholic fermentation promote its synthesis and then it is exported outside the yeast cell. From the technological point of view, the use of yeast strains with low capability of synthesizing acetic acid is advantageous. Temperature is one of the most important parameter for the development of alcoholic fermentation since it can affect both the kinetics of the process in terms of duration and rate of fermentation and the final quality of the fermented beverage, i.e., production of secondary metabolites (Lafon-Lafourcade, 1983; Fleet and Heard, 1993). The use of low fermentation temperatures (10-15°C) are currently increasing since it enhances the production and retention of flavour volatiles for example in winemaking (Killian and Ough, 1979; Kunkee, 1984).

Shake-flask cultures exhibit oxygen limitation (van Dijken van den Bosch *et al.*, 1986; Gupta and Rao, 2003; Tolosa *et al.*, 2002), which likely affects fermentative metabolism of yeasts. Factors that

influence the oxygen transference to the surface of the liquid include flask volume/liquid volume ratio, diameter and length of the neck of the flask and even the type of plug or closure (Nikakhtari and Hill, 2006).

Statistical analysis of the results of flavour, taste and odour showed significant difference (P < 0.01) between the two types of fermented beverages. Results of panelists have ascribed to the beverage fermented statically with slightly taste to solventlike, little acidic and unbalanced sensory profile, but not unpleasant. On the other hand, they ascribed to the beverage fermented in agitation as "bodiless" referring to sensory character, lack of aroma and taste compounds. The beverage fermented statically had an overall sensory acceptability based on the attributes evaluated.

# 4.2 Batch cultivation in bioreactor under constant air flow

Batch cultivation with constant air flow regime allows keeping a constant supply of oxygen into the medium. Transfer of oxygen into the liquid phase depends on many parameters such as the geometry of the bioreactor, viscosity of the medium, agitation speed, number of baffles, temperature, etc. Only oxygen dissolved in the liquid phase is totally available for the yeast cells. In experiments carried out in this study, air flow rate of 0.28vvm was kept constant during the whole fermentation time. In figures 1, 2 and 3 there are shown the courses of oxygen consumption, cellular growth, change of pH and synthesis and utilisation of by-products. The oxygen is the most important parameter which determines the balance between the fermentative and respiratory activity in many yeasts. At oxygen concentration lower than the critical value, the rate of respiration depends on the concentration of oxygen in the medium (Johnson, 1976). In presence of oxygen as a limiting substrate, the relationship between the growth rate and the concentration of oxygen in the medium follows the Michaelis Menten kinetics (Johnson, 1976). Critical concentration of oxygen for yeasts normally is very low ranging about 0.12 mg/L at 20 oC (Furukawa et al., 1983; Burke et al., 1997). In Fig. 1 is shown that, after 60<sup>th</sup> hour the concentration of dissolved oxygen in the medium dropped to zero and, it remained at this value towards the 260<sup>th</sup> hour of cultivation. During this time the oxygen transferred to the liquid phase was totally consumed. Nevertheless, this value does not give information about the rate of oxygen consumption. In this case, measurement of the oxygen concentration in the oulet gas is required. The oxygen has low solubility in pure water (9.1mg/L, 20oC) and depends on the temperature and physico-chemical properties of the liquid medium (e.g. viscosity). The oxygen consumed is utilized mostly in respiration process (glucose oxidation), but also in non-respiratory pathways such as synthesis of sterols and unsaturated fatty acids, which are essential components of the cellular membrane (Rosenfeld and Beauvoit, 2003).

Under this condition sugars were early depleted, glucose was first consumed (towards 60<sup>th</sup> hour) and then fructose (towards 80<sup>th</sup> hour). Studies reported that glucose is preferentially metabolised when fermentations are conducted in media containing an equal concentration of glucose and fructose. In this case, glucose is utilized approximately two times faster than fructose (D'Amore *et al.*, 1989), oxygen would enhance their rapid utilisation. During the first stage (aerobic fermentation), production of ethanol, glycerol and acetic acid took place (figure 2). Acetic acid was produced from the first hours of fermentation and then it was totally consumed. *Saccharomyces cerevisiae* is a Crabtree positive

yeast so in presence of high sugar concentration fermentation takes place even when oxygen is Glucose and fructose available in the medium. were consumed from the beginning and, as soon as they were totally depleted the microbial population showed the first diauxia (80<sup>th</sup> hour), probably due to the consumption and hydrolysis of sucrose and, soon afterwards a second diauxia was observed when ethanol started being consumed  $(98^{th} \text{ hour})$ . In Sacharomyces cerevisiae glucose is utilised first and invertase secretion is repressed when the glucose concentration is higher than 20 g/L (Mwesigye and Barford, 1996). Sucrose utilisation involves its hydrolysis outside the yeast cell since localisation of invertase is outer membrane. The occurrence of diauxic growth and catabolite inactivation of enzymes involved in ethanol metabolism suggest that simultaneous utilization of ethanol and glucose occur in S. cerevisiae RIVE V 15-1-416 only when the concentration of sugar (glucose or fructose) in the medium is very low (Fig. 2).

Consumption of sugars during the aerobic fermentation resulted in high production of ethanol 42.3 g/L) and glycerol (max. 2.2 g/L) (max. before being aerobically consumed, indicating higher biomass production (Fig. 2). Barford (1981) observed that in the aerobic ethanol formation from glucose in batch cultures with Saccharomyces cerevisiae, all sugar was first consumed with simultaneous ethanol production, followed by a short lag phase and resumed growth on ethanol. This phenomenon is often called the diauxic growth. The lag phase is characterised by the induction of enzymes of the glyoxylate cycle and gluconeogenesis, which are needed for synthesis of C<sub>3</sub> -  $C_6$  compounds from ethanol and other  $C_2$  substrates

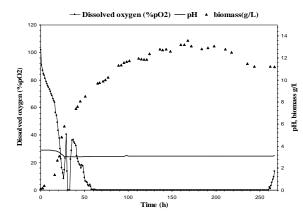


Fig. 1. Cultivation of *Saccharomyces cerevisiae* RIVE V 15-1-416 under constant air flow regime (0.28vvm) at 18°C.

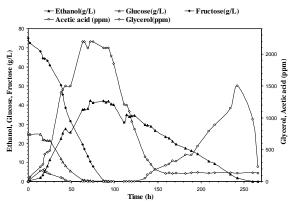


Fig. 2. Sugar consumption and metabolites produced during batch cultivation of *Saccharomyces cerevisiae*RIVE V 15-1-416 under constant air flow regime (0.28vvm) at 18°C.

(Haarasilta and Oura, 1975). The aerobic batch fermentation process can be described by low cell concentration (its maximum dropped to13.02 g/L dried cells) due to ethanol inhibition and a low biomass yield (0.11 g of biomass/g sugar) (see Table 2). The first stage of an aerobic fermentation is a consequence of a phenomenon called Crabtree effect (De Deken, 1966). In the presence of relatively low concentrations of glucose the expression of genes involved in the tricarboxylic acid cycle, oxidative phosphorylation, glyoxylate cycle, gluconeogenesis and metabolism of sugars other than glucose are repressed (Carlson, 1999; Gancedo, 1998). During aerobic growth of Saccharomyces cerevisiae on fermentable carbon sources, the fermentation/respiration is controlled as a response to the glucose level. Thus, this yeasts switch to a mixed respiro-fermentative metabolism, resulting in ethanol production, as soon as the external glucose concentration exceeds approx. 1mM (Verduyn *et al*, 1984). Higher ATP yield from the respiratory sugar dissimilation is reflected in the higher biomass yields of glucose limited cultures. Typical biomass yield obtained on glucose medium under respiration conditions is 0.5 g dry biomass per g consumed glucose; whereas the biomass yield of anaerobic, fermentative cultures is typically 5-fold lower (Verduyn, 1991). After sugar depletion, the ethanol and glycerol produced served as a carbon source for maintaining the cellular growth. From this stage of sugar depletion, concentration of dissolved oxygen dropped to zero and it remained almost constant towards the end of the cultivation. Acetic acid was produced again in higher concentration in a second stage during ethanol assimilation. Glycerol under this condition was mostly assimilated. Assimilation of acetic acid produced in the second stage started almost immediately after ethanol was totally consumed. Transport of ethanol and acetate may occur by passive diffusion; however, evidence for the existence of at least an acetate carrier has been obtained (Casal *et al.*, 1996). Increase of dissolved oxygen concentration in the liquid phase at the end of cultivation would be a result of carbon source depletion.

Production of glycerol by yeast cell would be mostly a response to increased osmolarity of the environment (osmoregulation) (Hohmann, 2002). Apple juice normally contains high sugar concentrations and it can provoke this phenomenon in S. cerevisiae RIVE V 15-1-416. Glycerol is a compatible solute produced in order to maintain the osmolarity inside the cells otherwise they would lose water and gradually it would slow down metabolic reactions inside the yeast cell. It was reported that, production of glycerol is controlled at the level of gene expression in yeasts (Hohmann, 1997; Gustin et al., 1998). To control properly gene expression, the cell has to detect (sense) osmotic changes and to transmit the signal to the nucleus. Then, a high osmolarity glycerol pathway is activated in S. cerevisiae (Gustin et al., 1998; Posas et al., 1998). Under aerobic conditions glycerol can be utilized as a carbon source. Thus, glycerol is converted into dihydroxyacetone phosphate, which subsequently enters the glycolytic or gluconeogenic pathway.

It was also observed that, the specific growth rate  $(0.13h^{-1})$  obtained during the first stage is typically noticed in fermentations carried out in media with high sugar concentrations (see table 2). Under glucose limitation and fully aerobic conditions the energy generated from the metabolism of glucose would be mostly used in cellular growth but, in cultivation conditions used in this study, part of the energy would be used in processes such as maintenance (Beeftink *et al.*, 1990).

Malic acid is the most important organic acid present in the apple juice; it contributes to the total acidity in ciders. The decrease of its content gives ciders better sensory quality. Wine yeasts in general cannot effectively degrade malic acid during alcoholic fermentation. Comercial wine yeasts of *Saccharomyces cerevisiae* are able to degrade only 18% of the malic acid (Redzepovic *et al.*, 2003). Results obtained in this study showed that, *S. cerevisiae* RIVE V 15-1-416 was able to utilise 36.0 % of the total malic acid present in apple juice. Nevertheless, degradation of malic acid by S. cerevisiae would depend on the strain. Presence of oxygen probably would enhance its utilisation as well. It was reported that some strains of S. cerevisiae could degrade significant quantities (up to 48%) of malic acid (Rainieri et al., 1998). It was also observed that degradation of malic acid started after sugar depletion (aerobic fermentation) and, simultaneously with ethanol assimilation (figure 3). Previous studies reported that, in S. cerevisiae, expression of the malic enzyme gene increases towards the end of fermentation as soon as glucose is depleted (Redzepovic et al., 2003). According to Salmon (1987), in S. cerevisiae yeasts malic and other dicarboxylic acids can be transported only via simple diffusion. Therefore due to at least transport limitations the yeasts are unable to degrade or utilise effectively extracellular malic acid. Succinic acid is the main organic acid produced by S. cerevisiae during metabolism of carbon source. It contributes to the taste of many alcoholic beverages such as for example in sake. Production of succinic acid during cultivation of S. cerevisiae RIVE V 15-1-416 in apple juice has attained values about 1.6 g/L (Fig. 3). In presence of oxygen, succinate is mainly synthesized through the tricarboxylic acid cycle (oxidative direction) even in presence of glucose at a concentration as high as 15% (Arikawa et al., 1999).

The variability of its synthesis observed during the course of the aerobic fermentation (Fig. 3) could be due to the fact that succinic acid is continuously excreted and imported in and out of the yeast cells. In presence of oxygen, succinic acid is an intermediary compound of the tricarboxylic acid cycle (TCA) during the complete oxidation of glucose. It was stated that, succinic acid could be synthesized through two pathways, namely,  $\alpha$ -ketoglutarate oxidation via the TCA cycle under aerobic conditions (oxidative direction) (Magarifuchi et al., 1995; Arikawa et al., 1999) and, fumarate reduction under anaerobic conditions (reductive direction) (Rossi et al., 1964; Wakai et al., 1980; Arikawa et al., 1999). Under slightly aerobic and glucose-depleted conditions, the glyoxylate cycle is a theoretically possible pathway for supplying succinate (Fernandez et al., 1992).

During aerobic fermentation, production of byproducts such as higher alcohols and acetate esters occurs. In experiments carried out in this study, residual concentrations of acetic acid, ethyl acetate and some higher alcohols at the end of cultivation (see Table 2) confirm that the sugar metabolism in the first part of the cultivation was predominantly fermentative. In the second stage (aerobic assimilation of ethanol) probably these higher alcohols served as carbon source

Initial conce	entration of sugars	s and malic acid (g/L)				
fructose 70.95	glucose 22.6	sucrose 35.5	malic acid 5.02			
Final compo	ounds (g/L)					
fructose traces	glucose traces	ethanol 0.0	glycerol 0.13±0.05	acetic acid 0.23±0.06	succinic ac. 1.5±0.3	malic acid 3.21±0.6
Higher alcol	hols and ethyl ace	etate produced (mg/L)				
1-propanol	propyl acetate	2-methyl propanol	3-methyl butanol	2-methyl butanol	Ethyl acetate	
1.2±0.04	6.8±0.12	1.0±0.04	1.6±0.05	1.03±0.05	2.1±0.06	
Sugar utilize	ed (S), final bioma	ass (X), yield $(Y_{X/S}, Y)$	(E/S), specific growth	n rate ( $\mu$ )		
S	Х	$Y_{X/S}$	$Y_{E/S}$	μ		
129.0	11.2	0.10	0.0	0.13		

Table 2. Compounds utilized and produced by *Saccharomyces cerevisiae* RIVE V 15-1-416 during batch cultivation under constant air flow regime at 18°C.

 $Y_{X/S}$ : g. of biomass/g. sugar;  $Y_{E/S}$ : g. of ethanol/g. sugar;  $\mu$ : specific growth rate (h<sup>-1</sup>); X: final dried biomass (g/l); S: total sugar consumed (g/L).

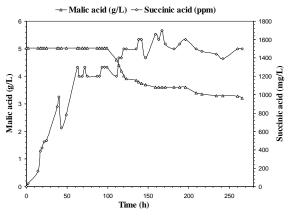


Fig. 3. Course of malic acid degradation and succinic acid synthesis in batch cultivation of *Saccharomyces cerevisiae* RIVE V 15-1-416 under constant air flow regime (0.28vvm) at 18°C.

in order to keep the growth of the cellular population. The low concentrations of higher alcohols found at the end of cultivation would support this suggestion (Table 2). From the technological point of view, fermentations should be stopped when the sugar is depleted or when the concentration of ethanol attains the inhibitory value. Excessive aeration during fermentation would lead to an increase in the cellular biomass concentration and as consequence of a decrease in ethanol production.

### Conclusions

Concentrations of sugar and dissolved oxygen are the most important factors that affect the metabolism of Saccharomyces cerevisiae. At high concentration of sugar (glucose), alcoholic fermentation takes place even when oxygen is present in sufficient amount. In agitated cultivations carried out in Erlenmeyer flasks, transfer of oxygen is a limiting factor since concentration of dissolved oxygen in the liquid phase is very low. Under this condition, presence of very low amount of oxygen affect the synthesis of fermentation by-products of Saccharomyces cerevisiae RIVE V 15-1-416. Oxygen has influenced the synthesis of glycerol, diminishes the synthesis of higher alcohols and on the contrary slightly increases the production of acetate esters such as ethyl acetate. These observations are controversial to those observed in cultivations carried out in similar conditions with some non-Saccharomyces yeast. The capability of synthesis of higher alcohols and esters under these conditions would also depend on the strain. Additionally, production of acetic acid diminished in agitated cultivation; it would be advantageous since alcoholic beverages with low volatile acidity are desirable. Temperature is an important factor that influences the metabolism of yeasts. It is known that high temperature of fermentation promotes a major production of higher alcohols. From this point of view, fermentations at temperatures lower than 28°C would be suitable in order to diminish production of higher alcohols. From the sensory point of view, static cultivation resulted in fermented beverages of better sensory acceptability and the best alternative to carry out fermentation of apple juice.

In batch cultivations carried out at constant air flow (0.28vvm), sugars are depleted towards the first three days of cultivation. Consumption of oxygen during this stage enhances the yeast growth and as a consequence the speed of fermentation but, on the contrary affects the yield of ethanol. In this case, excessive aeration should be avoided in order to improve the ethanol yield. On the other hand, a diauxic growth is observed when *S. cerevisiae* RIVE V 15-1-16 is grown in medium containing different carbon sources such as glucose, sucrose and ethanol. This phenomenom is a result of the short adaptation to a new carbon source.

Saccharomyces cerevisiae RIVE V 15-1-416 normally produces acetic acid and glycerol during aerobic fermentation, moreover, acetic acid is then consumed under this condition.

From the technological point of view, control of aeration rate would be a useful tool to reduce the concentration of acetic acid in ciders or other fermented beverages but, on the other hand, oxygen would increase synthesis of succinic acid. In consequence, reduction of volatile acidity and increase of non-volatile acids is somehow still beneficial. The aerobic fermentation process must be carefully controlled since after depletion of sugars, ethanol serves as carbon source. In this case, the process should be stopped once the maximum ethanol concentration has been attained. S. cerevisiae RIVE V 15-1-416 is not able to use malic acid during aerobic fermentation when fermentable sugars are still present in the medium. The continuous air flow to the medium once the aerobic fermentation has finished would not be suitable since it leads to the ethanol consumption. Finally, oxygen plays a very important role in the metabolism of S. cerevisiae RIVE V 15-1-416 and from the technological point of view only small amounts would be suitable in order to control the synthesis of fermentation by-products if production of alcoholic beverages is the purpose.

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